How to Cite:

Abdülhamit, A. (2024). Tubular chemical reactor theory to an arrangement of algebraic equations. *Tennessee Research International of Social Sciences*, *6*(1), 1-12. Retrieved from http://triss.org/index.php/journal/article/view/20

Tubular chemical reactor theory to an arrangement of algebraic equations

Ahmet Abdülhamit

Metu Middle East Technical University, Çankaya/Ankara, Turkey

Abstract---An operational framework of coordination is inferred and is utilized to decrease the model for an adiabatic tubular Chemical Reactor Theory to an arrangement of algebraic equations. Simple execution, basic activities, and precise arrangements are the basic highlights of the proposed wavelets technique. The numerical outcomes gotten by the present technique have been contrasted and compared with other strategy results. This paper exhibits an ancient numerical strategy of comprehending mathematical model for an adiabatic tubular chemical reactor which forms an irreversible exothermic chemical reaction. For enduring state solution for an adiabatic rounded concoction reactor, the model can be diminished to a conventional differential equation with a parameter in the limit conditions which changed over into a system of nonlinear equation that can be tackled numerically utilizing Taylor wavelets technique (TWM).

Keywords---Arrangement of algebraic, Tubular chemical, Exothermic chemical, Nonlinear equation.

Introduction

We propose a scientific model that has been created for an adiabatic tubular chemical reactor [1] which forms an irreversible exothermic chemical reaction. The model can be diminished to the second order differential equation with a parameter in the boundary conditions [2] in steady state arrangement as pursue:

$$\mathcal{V} - \mathcal{V} + (-\mathcal{V})e^{\mathcal{V}} = 0, \tag{1}$$

with the limit conditions

$$\mathcal{V}'(0) = \mathcal{V}(0), \qquad \mathcal{V}'(1) = 0.$$
 (2)

Tennessee research international of social sciences © 2024.

ISSN: 2766-7464 (Online)

Publisher: Smoky Mountain Publishing

Manuscript submitted: 09 Feb 2024, Manuscript revised: 18 March 2024, Accepted for publication: 27 April 2024

Wherever,

- v: symbolize the consistent state temperature of the reaction which must be resolved,
- μ : is the Damkohler number,
- β : is the adiabatic temperature ascent,
- λ is the Peclet number.

We postulate $\lambda > 0$, $\mu > 0$ and β 0. This issue has been contemplated by numerous specialists [1–4]. The steady state temperature of the reaction occurs when the solution of \mathcal{V} is positive. Wavelets are special kinds of oscillatory functions with compact support that provide the basis for numerous important spaces. They have been connected to a wide scope of issues in science and building disciplines. Wavelets are utilized in system investigation, ideal control, numerical examination, flag examination for waveform portrayal and division, time-recurrence examination and quick calculations for simple usage [5] the wavelets procedures have been getting more consideration of late to unravel differential and integral equations [6-7]. Hammerstein integral equations have been unraveled by numerous creators in [8–13] Haar wavelets was chiefly utilized to solve differential equations in [14].

A critical proportion of research work has been enhanced the circumstance the examination of a model for an adiabatic tubular Chemical Reactor theory, inclusive B-spline Wavelet technique [15], an algorithm dependent on Chebyshev development [16] and Adomian decomposition technique [17].

The diagram of this paper is as per the following: In Section 2, we present some essential definitions of wavelets, and we develop Taylor wavelets. In Section 3, Taylor wavelets operational matrix of integration is acquired, and in Section 4, Convergence test of the presented method. Section 5 is dedicated to the numerical technique for settling the Chemical Reactor theory. Numerical examples are given in Section 6 to illustrate the applicability and accuracy of our method. Finally, concluding remarks are given.

Fundamentals and Documentation

Wavelets and Taylor Wavelets

Wavelets are a group of capacities developed from widening and interpretation of a solitary capacity called the mother wavelet. At the point when the widening parameter τ and the interpretation parameter v change ceaselessly, we have the accompanying group of persistent wavelets as [18-21].

$$\psi_{\tau,\varphi}(x) = |\tau|^{\frac{-1}{2}} \psi\left(\frac{x-\varphi}{\tau}\right), \tau, \varphi \in R, \tau \neq 0$$
(3)

If we straiten the parameters τ and v and to distinguished values as $\tau = \tau_0^{-k}$, $\varphi = n\varphi_0\tau_0^{-k}$, $\tau_0 > 1$, $\varphi_0 > 1$ integer, the family of distinguished wavelets are:

2

$$\psi_{k,n}(x) = \left|\tau_0^{-k}\right|^{\frac{-1}{2}} \psi\left(\frac{x - n\varphi_0 \tau_0^{-k}}{\tau_0^{-k}}\right) = \left|\tau_0\right|^{\frac{k}{2}} \psi\left(\tau_0^k x - n\varphi_0\right)$$
(4)

Wherever $\psi_{k,n}(x)$ compose a wavelet rule for $L^2(R)$. TW $_{k,n}(x) = H(k, \hat{n}, m, x)$ have four arguments: $\hat{n} = n - 1$, $n = 1, 2, ..., 2^{k-1}$, k can expect any positive integer, m is the order for Taylor polynomials and x is the standardized time. We define them as in [22]:

$$\mathbf{H}_{n,m}(x) = \begin{cases} 2^{\frac{k-1}{2}} \mathbf{T}_m(2^{k-1}x - \hat{n}), & \frac{\hat{n}}{2^{k-1}} \le x < \frac{\hat{n}+1}{2^{k-1}}, \\ 0, & otherwise \end{cases}$$
(5)

$$\mathcal{F}_m(x) = \sqrt{2m+1} x^m. \tag{6}$$

Wherever m = 0, 1, 2, ..., M - 1 and $n = 1, 2, ..., 2^{k-1}$. The coefficient $\sqrt{2m + 1}$ is for normality, the dilation parameter is $\tau = 2^{-(k-1)}$ and the translation parameter is $\varphi = \hat{n}2^{-(k-1)}$.

Function Approaches

Suppose $u(x) L^{2}[0,1]$ can be extended with the TWM as:

$$u(x) = \sum_{n=1}^{\infty} \sum_{m=0}^{\infty} c_{nm} H_{nm}(x).$$
(7)

We can consider the following truncated series for f(x):

$$u(x) = \sum_{n=1}^{2^{k-1}} \sum_{m=0}^{M-1} c_{nm} \operatorname{H}_{nm}(x).$$
(8)

Wherever *T* indicates transposition, and *C*, $\psi(x)$ are $\hat{m} \times 1$ ($\hat{m} = 2^{k-1} M$) matrices given by

$$C = [c_{1,0}, c_{1,1}, \dots, c_{1,M-1}, c_{2,0}, \dots, c_{2,M-1}, \dots, c_{2^{k-1},0}, c_{2^{k-1},M-1}]^T$$
(9)
(x) = $[_{1,0'1,1}, \dots, c_{1,M-1'2,0}, \dots, c_{2^{M-1},M-1}, \dots, c_{2^{k-1},0}, c_{2^{k-1},M-1}]^T$ (10)
And $c_{nm} = \int_0^1 u(x) \check{H}_{nm}(x) dx$

TWM Operational Matrix of Integration

Utilizing the operational matrix of integration to eliminate integral operations. This matrix can be uniquely determined based on the orthogonal functions. The main objective of this section is to derive a TWM operational matrix of integration. Let (x) be the TW vector defined in Eq. (5), subsequently,

$$I(x) = P(x) \tag{11}$$

Wherever I and P are the integral operator and the $\hat{m} \times \hat{m}$ operational matrix of integration, respectively.

Utilizing Eq. (5), for $i = 1, \dots, 2^{k-1}$ and $j = 0, 1, \dots, M-1$, we have

$$I(\mathcal{H}_{ij}(x)) = I(2^{\frac{k-1}{2}}\sqrt{2j+1}(2^{k-1}x-\hat{\iota})\zeta_{[\frac{\hat{\iota}}{2^{k-1}},\frac{\hat{\iota}+1}{2^{k-1}}]}(x))$$
(12)

Wherever $\zeta_{[\frac{\hat{l}}{2^{k-1}},\frac{\hat{l}+1}{2^{k-1}}]}(x)$ is the distinctive result realized as:

$$\zeta_{\left[\frac{\hat{i}}{2^{k-1}},\frac{\hat{i}+1}{2^{k-1}}\right]}(x) = \begin{cases} 1, & \frac{\hat{i}}{2^{k-1}} \le x \le \frac{\hat{i}+1}{2^{k-1}} \\ 0, & otherwise \end{cases}$$
(13)

While $\hat{i} = i - 1$ Subsequently, in Eq. (12), for i = 1, we have

$$(2^{k-1}x - \hat{\imath})^{j} = \sum_{r=0}^{j} {j \choose r} 2^{(k-1)r} x^{r} (-1)^{j-r} \hat{\imath}^{j-r} I(x^{r} \zeta_{[\frac{\hat{\imath}}{2^{k-1}}, \frac{\hat{\imath}+1}{2^{k-1}}]}(x))$$
(14)

It is realized that

$$(2^{k-1}x - \hat{\imath})^{j} = \sum_{r=0}^{j} {j \choose r} 2^{(k-1)r} x^{r} (-1)^{j-r} \hat{\imath}^{j-r}$$
(15)

Hence, by subrogate Eq. (15) in Eq. (12) for $i = 2,3, \dots, 2^{k-1}$ we have

$$I(H_{ij}(x)) = 2^{\frac{k-1}{2}} \sqrt{2j+1} \sum_{r=0}^{j} {j \choose r} 2^{(k-1)r} (-1)^{j-r} \hat{\iota}^{j-r} I(x^r \zeta_{\left[\frac{\hat{\iota}}{2^{k-1}}, \frac{\hat{\iota}+1}{2^{k-1}}\right]}(x))$$
(16)

Now, approximating $I(x^r \zeta_{\left[\frac{\hat{l}}{2^{k-1}},\frac{\hat{l}+1}{2^{k-1}}\right]}(x))$ by \hat{m} terms of TW, we have

$$I\left(x^{r}\zeta_{\left[\frac{1}{2^{k-1}},\frac{1}{2^{k-1}}\right]}(x)\right) = h_{ir}(x) \simeq \sum_{n=1}^{2^{k-1}} \sum_{m=0}^{M-1} c_{nm}^{ir} H_{nm}(x) = C_{ir}^{T} H(x) \quad (17)$$
$$c_{ir}^{T} = D^{-1} < h_{ir}(x), H(x) >, D = < H(x), H(x) >$$

Subrogate Eq. (17) into Eqs. (14) and (16), we procure

$$I(H(x)) \simeq 2^{\frac{k-1}{2}} \sqrt{2j+1} 2^{(k-1)j} \sum_{n=1}^{2^{k-1}} \sum_{m=0}^{M-1} c_{nm}^{ij} H_{nm}(x)$$
$$= \sum_{n=1}^{2^{k-1}} \sum_{m=0}^{M-1} \varepsilon_{nm}^{1j} H_{nm}(x), j = 0, 1, \dots, M-1,$$
(18)

And

$$I(H_{ij}(x)) = 2^{\frac{k-1}{2}} \sqrt{2j+1} \sum_{r=0}^{j} {j \choose r} 2^{(k-1)r} (-1)^{j-r} \hat{\iota}^{j-r} \sum_{n=1}^{2^{k-1}} \sum_{m=0}^{M-1} c_{nm}^{ij} H_{nm}(x) \quad (19)$$

$$= \sum_{n=1}^{2^{k-1}} \sum_{m=0}^{M-1} \varepsilon_{nm}^{ij} H_{nm}(x), i = 2, 3, ..., 2^{k-1}, j = 0, 1, ..., M - 1,$$

$$\varepsilon_{nm}^{1j} = 2^{\frac{k-1}{2}} \sqrt{2j+1} 2^{(k-1)j} c_{nm}^{1j}$$

And

$$\varepsilon_{nm}^{ij} = 2^{\frac{k-1}{2}} \sqrt{2j+1} \sum_{r=0}^{j} {j \choose r} 2^{(k-1)r} (-1)^{j-r} \hat{\iota}^{j-r} c_{nm}^{ir}$$

Therefore, we get

$$P = \begin{pmatrix} \varepsilon_{10}^{10} & \dots & \varepsilon_{1M-1}^{10} & \dots & \varepsilon_{2^{k-1}0}^{10} & \dots & \varepsilon_{2^{k-1}M-1}^{10} \\ \varepsilon_{10}^{11} & \dots & \varepsilon_{1M-1}^{11} & \dots & \varepsilon_{2^{k-1}0}^{11} & \dots & \varepsilon_{2^{k-1}M-1}^{11} \\ \vdots & \vdots & \vdots & \vdots & \vdots & \vdots & \vdots \\ \varepsilon_{10}^{2^{k-1}M-1} & \dots & \varepsilon_{1M-1}^{2^{k-1}M-1} & \dots & \varepsilon_{2^{k-1}M-1}^{2^{k-1}M-1} \end{pmatrix}$$
(20)



Fig.1. Patterns of the matrices D (right) and P (left) at k = 2 and M = 3.

Convergence Test

Theorem

We postulate that $u \in C^2[0,1]$ is represented by TWM, where has 2 vanishing moments.

Subsequently $|c_{j,k}| \le \alpha \beta \xi^2 \frac{2^{-3j}}{2!}$, wherever $\alpha = max |u''(t)|, \beta = \int_{-k}^{2^{j-k}} \check{H}(x) dx$ and $\xi \in (-k, 2^j - k)$. Proof. Taylor expansion of $f \in C^2[0,1]$ about arbitrary $x_0 \in [0,1]$ Can be written as:

$$u(x) = u(x_0) + u'(x_0)(x - x_0) + \frac{(x - x_0)^2}{2!}u''(\delta_0), \delta \in (0, 1).$$
(21)

Here u(x) can be specified by TWM as:

$$u(x) = C^{T}(x)$$

Wherever

$$c_{j,k} = \int_0^1 u^T \breve{\mathbf{H}}_{j,k}(x) dx \tag{22}$$

Putting Eq. (21) in Eq. (22), we get

$$c_{j,k} = \int_0^1 u(x_0) \breve{H}_{j,k}(x) dx + \int_0^1 (x - x_0) u'(x_0) \breve{H}_{j,k}(x) + \int_0^1 \frac{(x - x_0)^2}{2!} u''(\delta) \breve{H}_{j,k}(x) dx$$
(23)

Laying $x_0 = \frac{k}{2^j}$ and $f = 2^j x - k$ in Eq. (29), we have

$$c_{j,k} = 2^{-j} u\left(\frac{k}{2^{j}}\right) \int_{-k}^{2^{j}-k} \breve{H}_{j,k}\left(f\right) df + \int_{-k}^{2^{j}-k} f \,\breve{H}_{j,k}\left(f\right) df + \frac{u''(\delta)}{2!} 2^{-3j} \int_{-k}^{2^{j}-k} f^{2} \,\breve{H}_{j,k}\left(f\right) df$$
(24)

Suppose T is a linear transformation such that

Subsequently starting the transformation T of the two integral of Eq. (24) we have

$$c_{j,k} = 2^{-j}u\left(\frac{k}{2^{j}}\right)\int_{-k}^{2^{j}-k} T(\mathcal{H}_{j,k}(f))du + 2^{-j}u'\left(\frac{k}{2^{j}}\right)\int_{-k}^{2^{j}-k} uT(\mathcal{H}_{j,k}(f))df + \frac{u''(\delta)}{2!}2^{-3j}\int_{-k}^{2^{j}-k} f^{2}\,\widetilde{\mathcal{H}}_{j,k}(f)df$$
(25)

$$c_{j,k} = 2^{-j} u\left(\frac{k}{2^{j}}\right) T \int_{-k}^{2^{j}-k} \mathbf{H}_{j,k}(f) du + 2^{-j} u'\left(\frac{k}{2^{j}}\right) T \int_{-k}^{2^{j}-k} f(\mathbf{H}_{j,k}(f)) df + \frac{u''(\delta)}{2!} 2^{-3j} \int_{-k}^{2^{j}-k} f^{2} \breve{\mathbf{H}}_{j,k}(f) df$$

According to vanishing moments of order *m*, i.e. $\int_{-\infty}^{\infty} x^p \operatorname{H}(x) dx = 0$, $p = 0, 1, \dots, m - 1$, Subsequently, from (25) we have

$$c_{j,k} = \frac{u''(\delta)}{2!} 2^{-3j} \int_{-k}^{2^j - k} f^2 \,\breve{\mathsf{H}}_{j,k}(f) df \tag{26}$$

Stratifying the mean value theorem for integral in Eq. (26), we have

$$c_{j,k} = \frac{u''(\delta)}{2!} 2^{-3j} \xi^2 \int_{-k}^{2^j - k} f^2 \, \check{\mathrm{H}}_{j,k}(f) df, \ \xi \epsilon(-k, 2^j - k) \tag{27}$$

Hence

$$\begin{vmatrix} c_{j,k} \end{vmatrix} \le \alpha \beta \xi^2 \frac{2^{-3j}}{2!}$$
(28)

Application of the TWM to the Adiabatic Tubular Chemical Reactor

In this portion, we have resolved the model characterized in Eq. (3) utilizing TWM. Initially, we postulate:

$$\mathcal{V}(x) = C^{T}(x), \ 0 \le x \le 1$$
 (29)

Now from Eq. (37), we can approximate the functions $\mathcal{V}(x)$ as

$$\mathcal{V}(\mathbf{x}) = \mathbf{C}^T \, \mathbf{p}(\mathbf{x}) + \mathbf{y}(\mathbf{0}) \, \mathbf{d}^T \, \mathbf{p}(\mathbf{x}) \tag{30}$$

And

$$\mathcal{V}(x) = \mathbf{C}^T \mathbf{P}^2 \operatorname{H}(x) + \mathcal{V}'(\mathbf{0}) \, \mathbf{d}^T \, \mathbf{p} \operatorname{H}(x) + \mathcal{V}(\mathbf{0}) \tag{31}$$

Wherever p is the TWM operational matrix of integration. Subrogate Esq. (29-31) in Eq. (1), we get

$$C^{T}H(x) - C^{T}p H(x) - \mathcal{V}'(0) d^{T}p H(x) + (\beta - C^{T}P^{2} H(x) + \mathcal{V}'(0) d^{T}p H(x) + \mathcal{V}(0))e^{(C^{T}P^{2} H(x) + \mathcal{V}'(0) d^{T}p H(x) + \mathcal{V}(0))} = 0$$
(32)

Next, we arrange the Eq. (32) that yield \hat{m} nonlinear equations which can be illuminated for the obscure vector *C* by Newton's iterative procedure. The initial and boundary value problems emerging in the theory of gases and elasticity are diminutive to nonlinear shape to solve them. Due to their significant importance, numerous numerical and analytical strategies have been created for these issues due to it is not sensible to deduce its exact solution by an algebraic operation, for instance, iterative numerical solvers dependent on Newton's method [23–28]. It is notable that the underlying estimates for Newton's iterative system are imperative. A strategy like [29] can be utilized for picking the underlying estimates.

$$y_{n} = x_{n} - \frac{2y(x_{n})y'(x_{n})}{2y'^{2}(x_{n}) - y(x_{n})y'(x_{n})}$$
(33)
$$x_{n+1} = x_{n} - \frac{2(y(x_{n}) + y(y_{n}))y'(x_{n}))}{2y'^{2}(x_{n}) - (y(x_{n}) + y(y_{n}))y'(x_{n})}$$
(34)

The nonexclusive flow outline strategy is given in Fig. 1.



Fig.2. Schematic depiction of the suggested methodology for detecting the solution of nonlinear equations dependent on variations of germinal algorithms

present procedure and the strategies are given in ref. [2] (i.e. Adomian's decomposition method, Contraction mapping principle and Shooting method). Since the correct arrangement of this issue isn't known, from the figure it manifests that we get accurate results by TWM at k = 2, M = 3 in contrast with different techniques. We will get a more accurate result by increasing the value of k, M. To approve the utilization of TWM to (1), (2), we utilize specific estimations of the parameters at ($\lambda = 10$, $\beta = 3$ and = 0.02) as demonstrated in figure 3.



Fig.3. Numerical results acquired by twm at k = 2, M = 3,with the results of other available techniques in ref. [3]

Table 1: Comparison of numerical results acquired by TWM at k = 2, M = 3, with the results of other technique (B-spline wavelet method, Adomian's technique, the contraction mapping principle, Shooting technique and Sinc-Galerkin with $\lambda = 10$, $\beta = 3$ and 2000

	TWM at	B-spline				ChFD	Sinc-	Sinc-
x	k=2,	wavelet		Shooting	CMP	Method	Galerkin	Galerkin
	M = 3	method	ADM	Method			at <i>N</i> = 10	at N = 20
0	0.006048	0.006045	0.006048	0.006048	0.006048	0.006048	0.006049	0.006048
0.2	0.018192	0.018194	0.018192	0.018192	0.018192	0.018192	0.018197	0.018192
0.4	0.030424	0.030424	0.030424	0.030424	0.030424	0.030424	0.030437	0.030424
0.6	0.042669	0.042675	0.042669	0.042669	0.042669	0.042669	0.042649	0.042669
0.8	0.054371	0.054332	0.054371	0.054371	0.054371	0.054371	0.054383	0.054371
1	0.061458	0.062030	0.061458	0.061458	0.061458	0.061458	0.061459	0.061458

As appeared in Table 1, the outcomes utilizing present technique with k = 2, M = 3 concur with those of the B-spline wavelet method, Shooting method, ChFD method, Sinc-Galerkin at N = 20 and ADM up to the sixth decimal place.

Conclusion

We have built up a model for an adiabatic tubular chemical reactor theory utilizing TWM at k = 2, M = 3. The operational matrix of integration of TW is determined and utilized to reduce the solution of the adiabatic tubular chemical reactor theory to a system of algebraic equations fathoms dependent on variants of Newton strategies. The numerical results acquired by present strategy have been compared with other numerical and semi-analytical technique acquired by Contraction mapping principle, shooting technique, Adomian's decomposition technique Shooting Method and Chebyshev finite difference technique. The strategy is computationally appealing and applications are shown through an illustrative paradigm.

References

- Al-Ali, K., Kodama, S., & Sekiguchi, H. (2014). Comparison of the performance of a direct-contact bubble reactor and an indirectly heated tubular reactor for solar-aided methane dry reforming employing molten salt. *Chemical Engineering and Processing: Process Intensification*, 83, 56-63.
- Amundson, N. R. (2014). The mathematical understanding of chemical engineering systems. Elsevier.
- Andreini, A., Ceccherini, A., Facchini, B., Turrini, F., & Vitale, I. (2009, January). Assessment of a set of numerical tools for the design of aero-engines combustors: study of a tubular test rig. In *Turbo Expo: Power for Land, Sea, and Air* (Vol. 48838, pp. 421-433).
- Bassingthwaighte, J. B. (1970). Blood flow and diffusion through mammalian organs: Stochastic methods used for chemical reactor analysis are readily applicable to complex biologic systems. *Science (New York, NY), 167*(923), 1347.
- Bonvin, D., Rinker, R. G., & Mellichamp, D. A. (1980). Dynamic analysis and control of a tubular autothermal reactor at an unstable state. *Chemical Engineering Science*, 35(3), 603-612.
- Calise, F., d'Accadia, M. D., & Restuccia, G. (2007). Simulation of a tubular solid oxide fuel cell through finite volume analysis: Effects of the radiative heat transfer and exergy analysis. *International Journal of Hydrogen Energy*, 32(17), 4575-4590.
- Caracotsios, M., & Stewart, W. E. (1995). Sensitivity analysis of initial-boundaryvalue problems with mixed PDEs and algebraic equations: applications to chemical and biochemical systems. *Computers & chemical engineering*, 19(9), 1019-1030.
- Crider, J. E., & Foss, A. S. (1966). Computational studies of transients in packed tubular chemical reactors. *AIChE journal*, *12*(3), 514-522.
- Dixon, A. G., Nijemeisland, M., & Stitt, E. H. (2006). Packed tubular reactor modeling and catalyst design using computational fluid dynamics. *Advances in Chemical Engineering*, *31*, 307-389.

- Fan, S., Gretton-Watson, S. P., Steinke, J. H. G., & Alpay, E. (2003). Polymerisation of methyl methacrylate in a pilot-scale tubular reactor: modelling and experimental studies. *Chemical engineering science*, 58(12), 2479-2490.
- Flores-Tlacuahuac, A., & Grossmann, I. E. (2011). Simultaneous cyclic scheduling and control of tubular reactors: Parallel production lines. *Industrial & engineering chemistry research*, *50*(13), 80868096.
- Fogler, H. S. (2010). Essentials of Chemical Reaction Engineering: Essenti Chemica Reactio Engi. Pearson Education.
- Georgiadis, M. C., & Macchietto, S. (2000). Dynamic modelling and simulation of plate heat exchangers under milk fouling. *Chemical Engineering Science*, 55(9), 1605-1619.
- Gilkeson, M. M., White, R. R., & Sliepcevich, C. M. (1953). Synthesis of Methane by Hydrogenation of Carbon Monoxide in a Tubular Reactor. *Industrial & Engineering Chemistry*, 45(2), 460-467.
- Häfele, M., Kienle, A., Boll, M., Schmidt, C. U., & Schwibach, M. (2005). Dynamic simulation of a tubular reactor for the production of low-density polyethylene using adaptive method of lines. *Journal of Computational and Applied Mathematics*, 183(2), 288-300.
- Hayes, R. E., & Mmbaga, J. P. (2012). Introduction to chemical reactor analysis. CRC Press.
- Hillestad, M. (2010). Systematic staging in chemical reactor design. *Chemical engineering science*, 65(10), 3301-3312.
- Hsuen, H. K. D. (1996). Effects of spatial discretization errors on the steady-state multiplicity of a onedimensional tubular reactor model with intraparticle transport. *Chemical engineering science*, 51(17), 4215-4218.
- Iordanidis, A. A. (2002). *Mathematical modeling of catalytic fixed bed reactors* (pp. 98-112). Enschede, The Netherlands: Twente University Press.
- Jakobsen, H. A. (2008). Chemical reactor modeling. Multiphase Reactive Flows.
- Khodayari, H., Ommi, F., & Saboohi, Z. (2020). A review on the applications of the chemical reactor network approach on the prediction of pollutant emissions. *Aircraft Engineering and Aerospace Technology.*
- Koppel, L. B. (1966). Dynamics and Control of a Class of Nonlinear, Tubular, Parametrically Forced Heat Exchanger and Chemical Reactors. *Industrial & Engineering Chemistry Fundamentals*, 5(3), 403413.
- Kubicek, M., & Holodniok, M. (1982). Two-Phase Model Of A Tubular Nonadiabatic Reactor With Axial Dispersion And Gas-To-Solid Heat And Mass Transfer. Numerical Methods For Steady State Analysis. In *International*
- Heat Transfer Conference Digital Library. Begel House Inc..
- Nájera, I., Álvarez, J., Baratti, R., & Gutiérrez, C. (2016). Control of an exothermic packed-bed tubular reactor. *IFAC-PapersOnLine*, 49(7), 278-283.
- Pareek, V. (2005). Light intensity distribution in a dual-lamp photoreactor. International Journal of Chemical Reactor Engineering, 3(1).
- Salmi, T. O., Mikkola, J. P., & Wärnå, J. P. (2019). Chemical reaction engineering and reactor technology. CRC Press.
- Sayer, C., Palma, M., & Giudici, R. (2002). Kinetics of vinyl acetate emulsion polymerization in a pulsed tubular reactor: comparison between experimental and simulation results. *Brazilian Journal of Chemical Engineering*, 19(4), 425-431.

- Schweiger, C. A., & Floudas, C. A. (1999). Optimization framework for the synthesis of chemical reactor networks. *Industrial & Engineering Chemistry Research*, 38(3), 744-766.
- Varma, A., & Amundson, N. R. (1973). Some observations on uniqueness and multiplicity of steady states in non-adiabatic chemically reacting systems. *The Canadian Journal of Chemical Engineering*, 51(2), 206-226.
- Zacca, J. J., & Ray, W. H. (1993). Modelling of the liquid phase polymerization of olefins in loop reactors. *Chemical Engineering Science*, 48(22), 3743-3765.
- Zavala, V. M., & Biegler, L. T. (2006). Large-scale parameter estimation in lowdensity polyethylene tubular reactors. *Industrial & engineering chemistry* research, 45(23), 7867-7881.
- Zheng, D., Hoo, K. A., & Piovoso, M. J. (2002). Low-order model identification of distributed parameter systems by a combination of singular value decomposition and the Karhunen- Loève expansion. *Industrial & Engineering Chemistry Research*, 41(6), 1545-1556.